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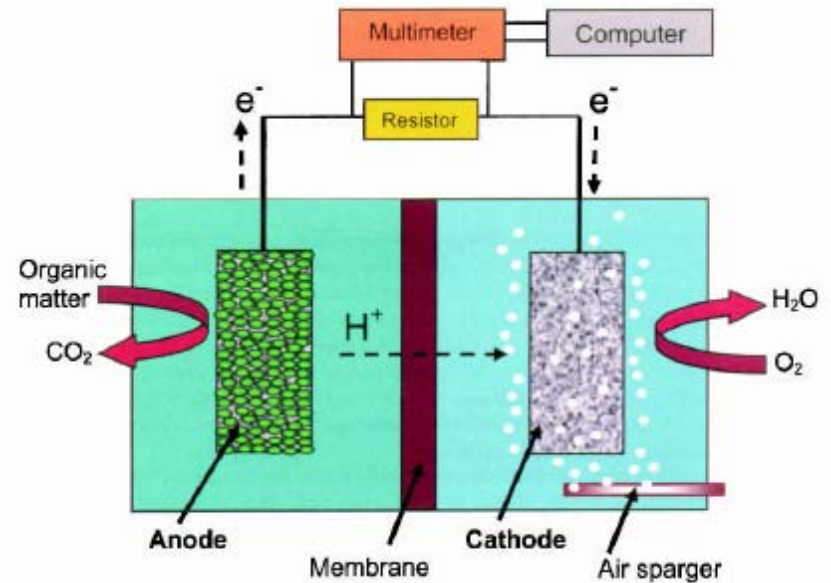
## Microbial Fuel Cell

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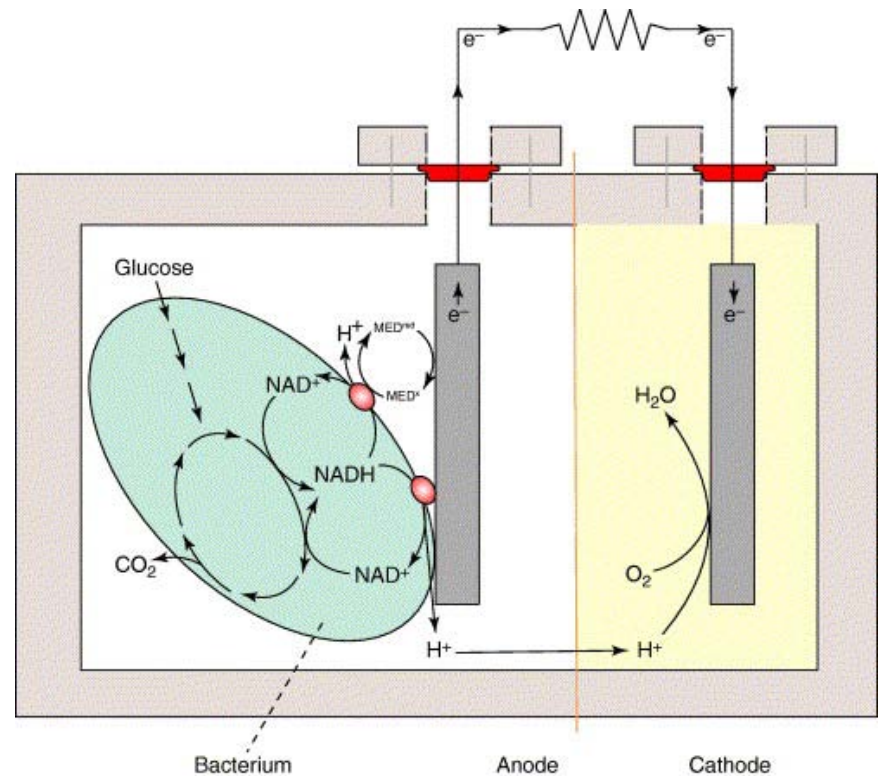
## ■ Microbial fuel cell (MFC)

- MFC's are devices that produce energy from bacteria (and other microbes) metabolism
- The devices involve an anode and a cathode
- In the anode bacteria's energy pathways are tapped into producing electrons and protons ( $H^+$ )
- $H^+$  crosses a PEM –  $H^+$  only barrier
- $H^+$  in the cathode are oxidized to produce water`



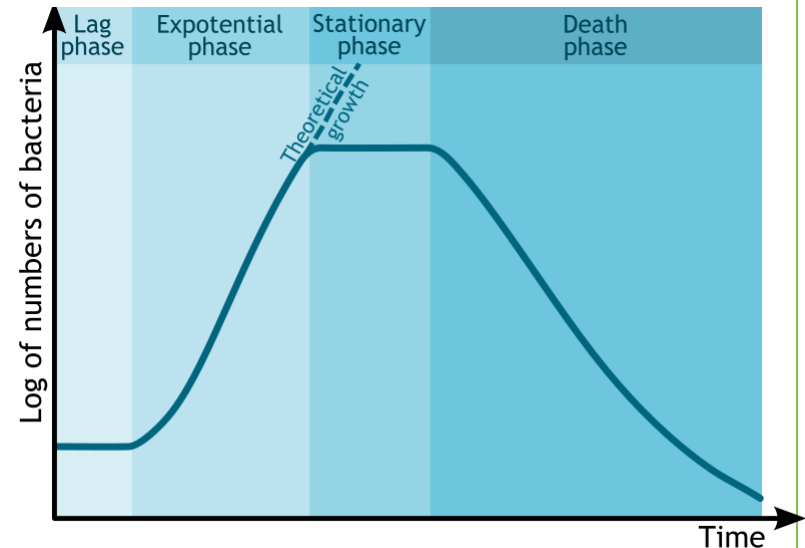
## Chemistry of electron production

- When microbes (in or case E. coli) metabolize glucose, intermediates are produced
- These intermediates along the energy pathway can give up an electron to an external molecule called a mediator
- The mediator undergoes a redox reaction, where the “trapped” electron is transferred to an electrode surface
- The mediator has the property traveling across the cell membrane



## Bacteria growth kinetics

- Bacteria growth is dependent, most rudimentary, on the presence of substrate/food and on temperature (pH and other nutrients are also crucial, but assumed present)
  - There are 4 phase characterizing bacteria growth
  - **Lag** – bacteria become accustomed to the environment
  - **Exponential** – rapid growth
  - **Stationary** – nutrient consumption leads to slowed growth
  - **Death** – lack of nutrients
- 
- The presence of bacteria then can be controlled through nutrient distribution and thermal energy (there is an optimal temperature for proper enzyme functioning)



## ■ Project objective

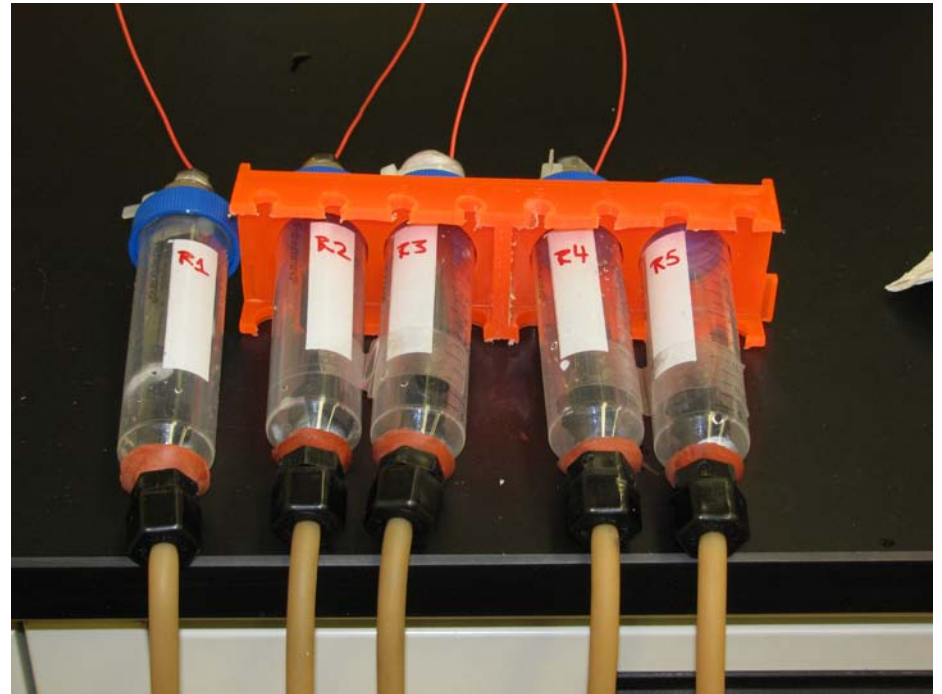
- In this project it is the goal to maintain an optimum bacteria population, and consequent current production through control of **thermal energy**
- The bacteria population is proportional to the current produced
- A PID algorithm, is used
- BS2 communicates with MATLAB's SIMULINK
- SIMULINK communicates with an automatic Heat exchanger via RS232 port

# Construction



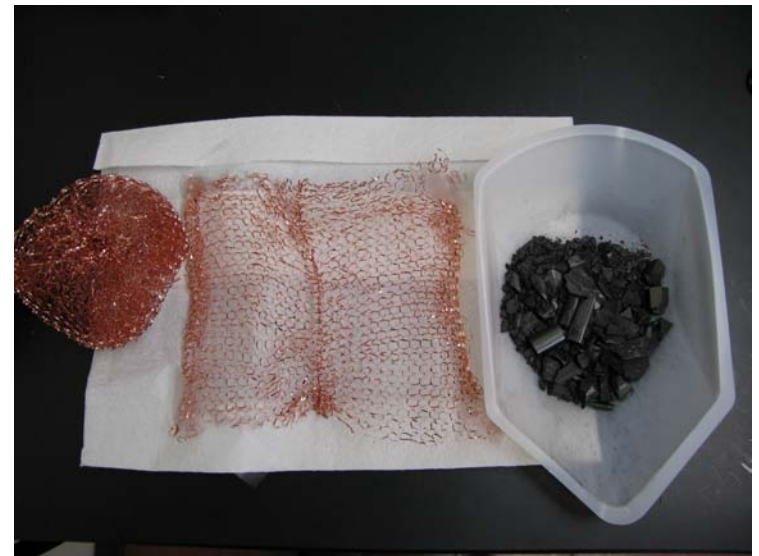
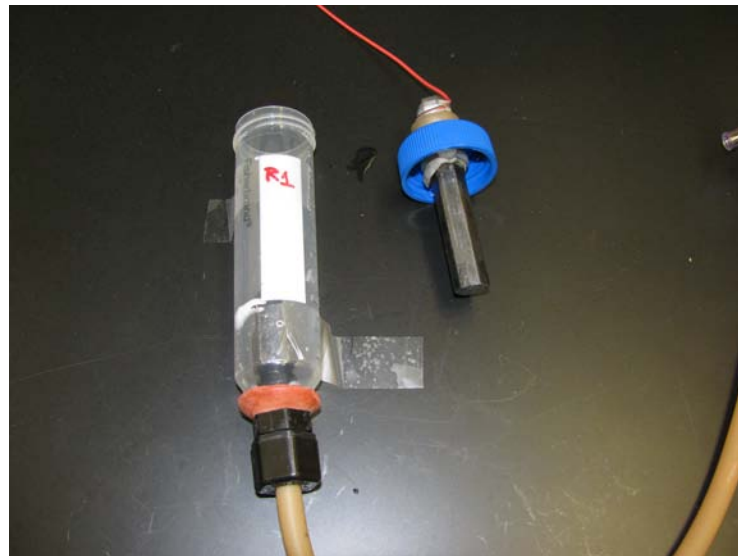
## ■ Design: Anode

- Five reactors are run simultaneously to increase current production in series
- Current of 0.025mA per  $\sim 4\text{m}^2$  and 5.1mV early in the lag phase
- Reaction volume of 35mL each\*
- On anode side, LB broth is used at pH 6.8
- Humic acid mediator was used at 5% volume
- Fe(III) used as sacrificial reducing agent



## ■ Design: Bio-compatible electrode

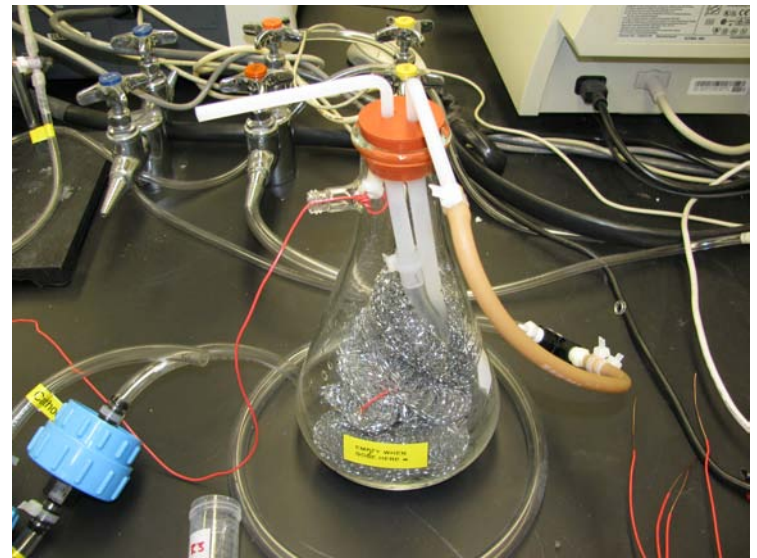
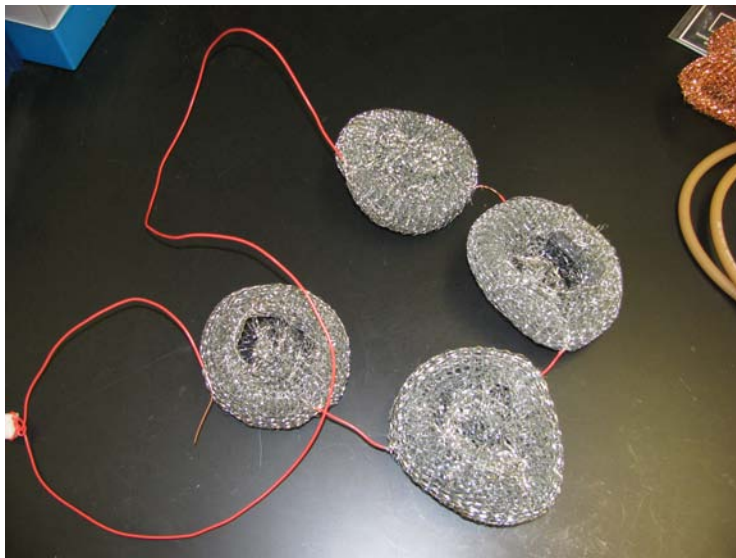
- A bio-compatible electrode is needed
- 100% Graphite was used in high surface to volume
- The Conductance of 12mm thick by 18cm length graphite electrode is comparable to metals





## ■ Design: Cathode

- Steel wool/low grade carbon steel is used as cathode catalyst
- This is used with a solution of Fe(III) (same concentration as in anode) to promote oxidation of H<sup>+</sup> at pH 2.1

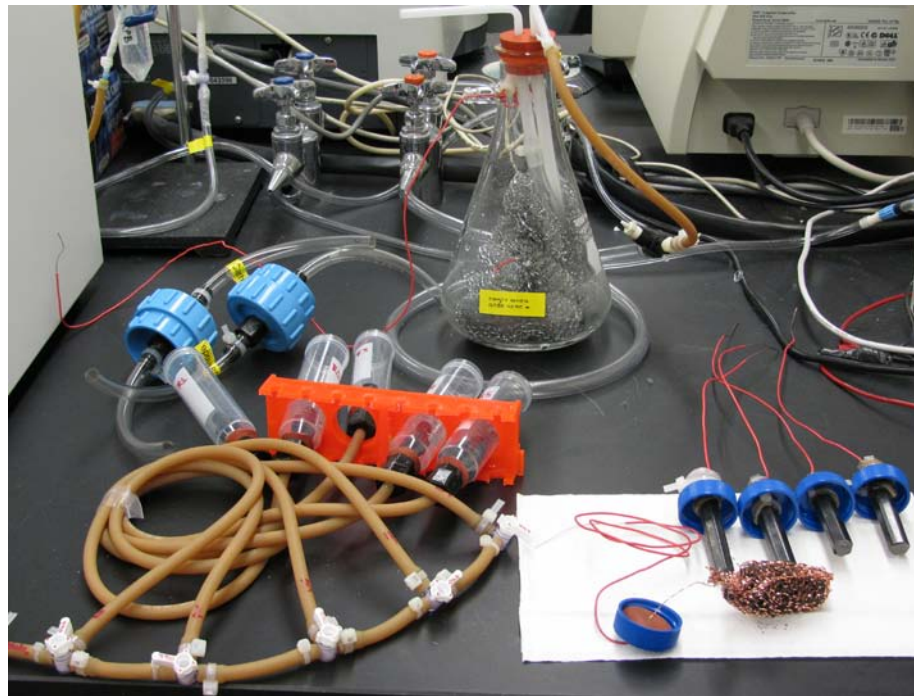


## ■ Proton exchange membrane

- We need a membrane that allows only H<sup>+</sup>/protons across
- Gortex is a common material with this property
- Gortex is held in place by a filter holder
- The Gortex interface is the bottle neck to current production
- Has the job of separating two phases of differing pH



## ■ Design: Construction



## Final setup

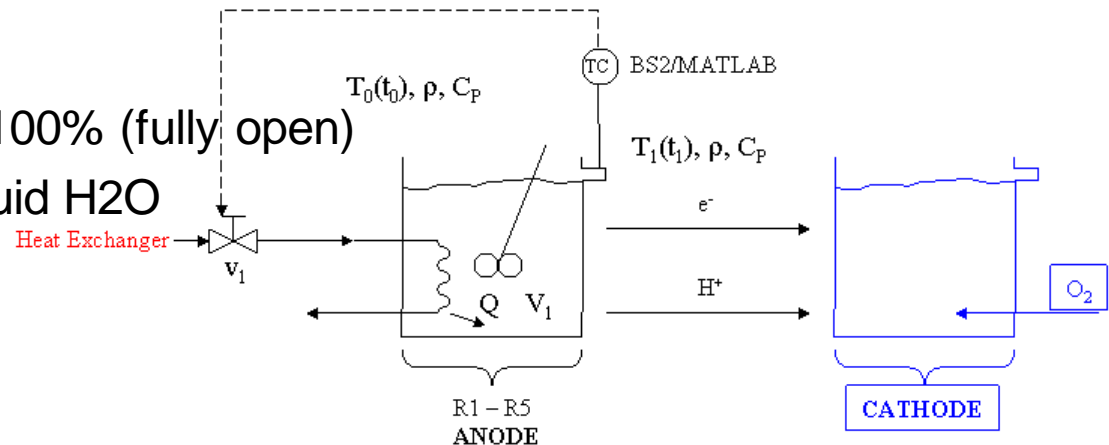


# Mechatronics Implementation



## ■ Process Model – Temperature Control

- The process is modeled as a 1st order system with deadtime.
- $V = 200\text{mL}$
- $F = 0.5\text{L/sec}$
- $T_{0,\text{init}} = 20\text{oC}$
- To range:  $0\text{oC}$  to  $100\text{oC}$
- Step =  $+60\text{oC}$
- Step time =  $100\text{sec}$
- Valve Position:  $0\%$  to  $100\%$  (fully open)
- Constant properties, fluid H<sub>2</sub>O





## ■ Simulink Open loop temperature disturbance

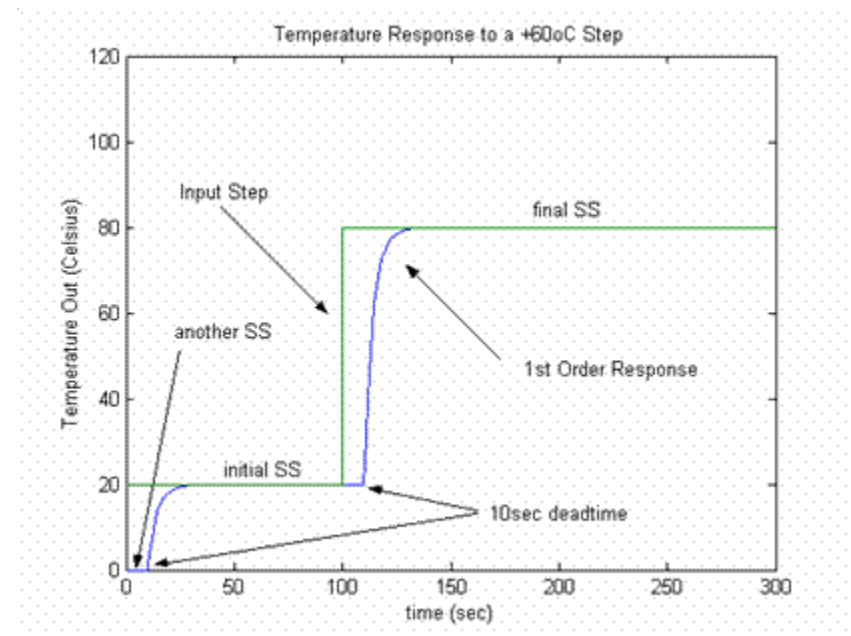
$$\frac{d}{dt}[mC_p T] = \frac{d}{dt}[\rho V C_p T] = \rho F C_p T_o - \rho F C_p T$$

$\rho, V$  are constant,  $C_p \approx C_p$

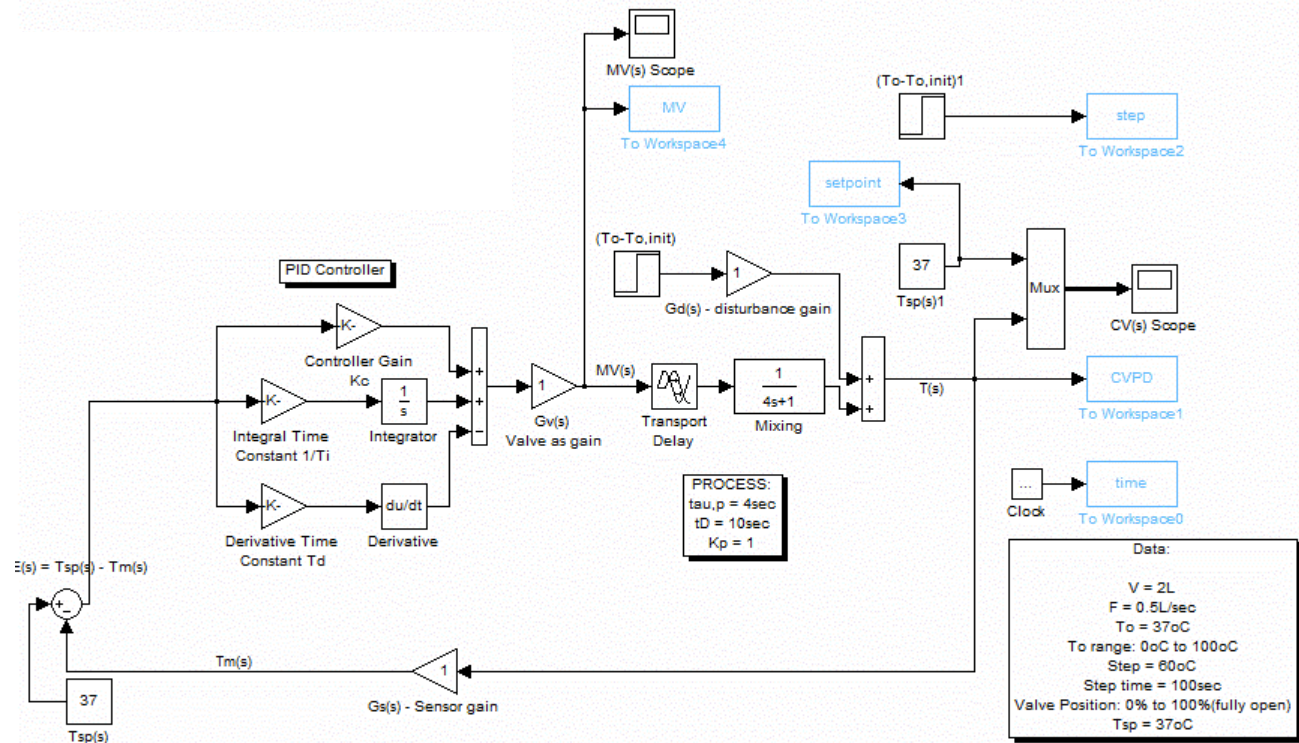
$$\tau \frac{dT}{dt} + T = K T_o$$

$$\tau = \frac{V}{F} \quad K = \frac{F \tau}{V}$$

$$G_p(s) \frac{T(s)}{T_o(s)} = \frac{K}{(\tau s + 1)}$$



## ■ Simulink Closed loop PID temperature control



### TEMPERATURE CONTROL

Process modelled as a first order system with delay; the simulation time is 300sec.





## ■ Simulink Closed loop temperature control

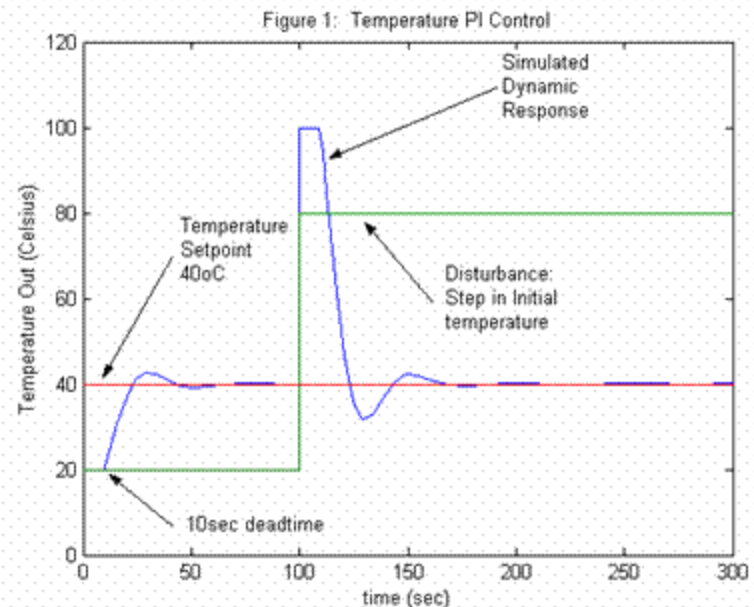
Controller Parameters:  
(Cohen & Coon)

**PID -  $K_c = 0.783$ ;  $T_i = 14.42\text{sec}$ ;  $T_d = 0.25\text{sec}$**

PI -  $K_c = 0.443$ ;  $T_i = 6.37\text{sec}$ ;  $T_d = 0$

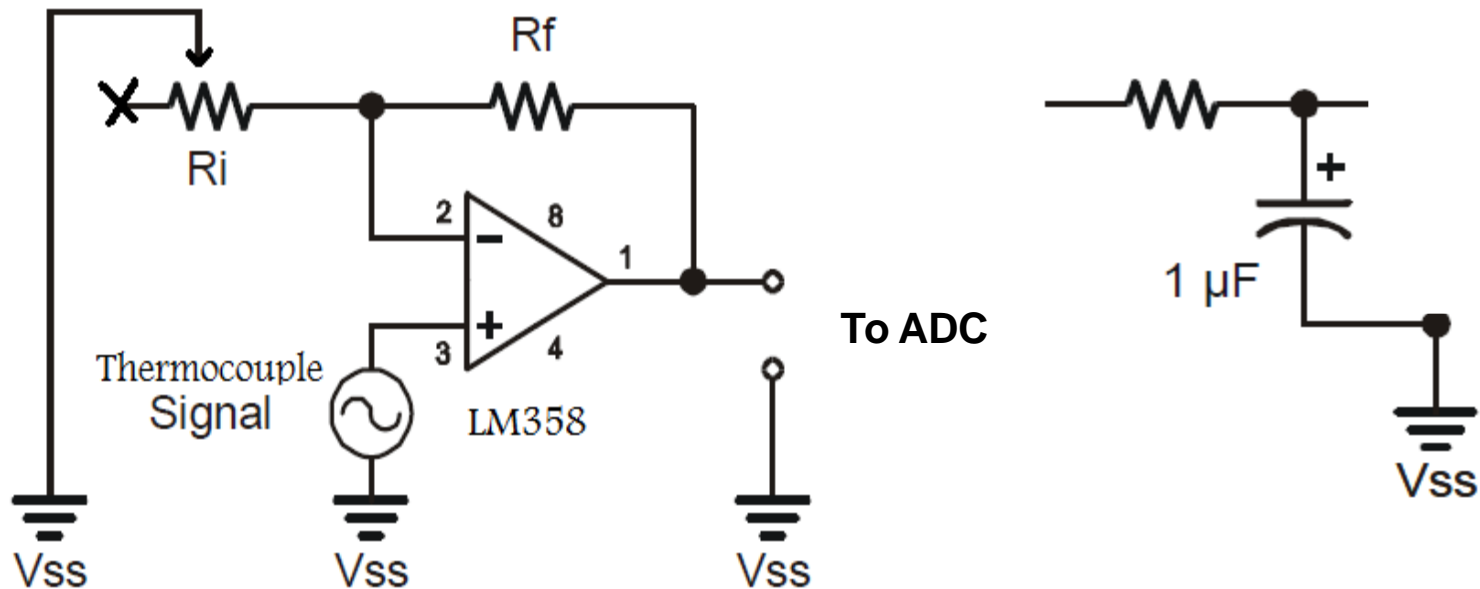
PD -  $K_c = 0.667$ ;  $(1/T_i) = 0$ ;  $T_d = 0.339\text{sec}$

P -  $K_c = 0.733$ ;  $(1/T_i) = 0$ ;  $T_d = 0$



## Sensor: Thermocouple

- Amplify thermocouple signal
- Filter out signal noise
- Calibrate the linear voltage to temperature scale



- Operational amplifier in non-inverting configuration
- Low pass filter used to reduce noise fluctuation

## ■ Sensor: Current sensor

- Vernier sensor can be interfaced with BS2 directly, through the 5 pins
- The current meter is used to measure current in parallel to the load
- In this experiment the load is a 10M $\Omega$  resistor
- 10 $\mu$ F capacitor used to eliminate noise in current produced
- According to manufacturer specifications, the heat exchanger is controlled



# Programming



# Now What?

